



Design and Scheduling of Flexible Processing Systems: An Optimization Approach

Ana Paula Barbosa Póvoa

**Centro de Estudos de Gestão, CEG-IST
Instituto Superior Técnico**

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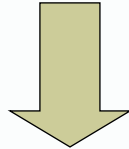
Overview

- Objective
- Flexible Processing Systems
- Problems & Challenges
- Systems Approach
 - Processes, Resources, Operating Conditions
- Generic Problems Representations
- Scheduling
- Design
- Supply Chains
- Conclusions & Future Work

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Objective

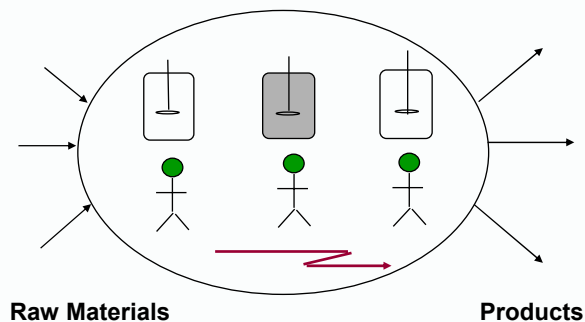
Develop generic models for the design and scheduling of flexible process systems



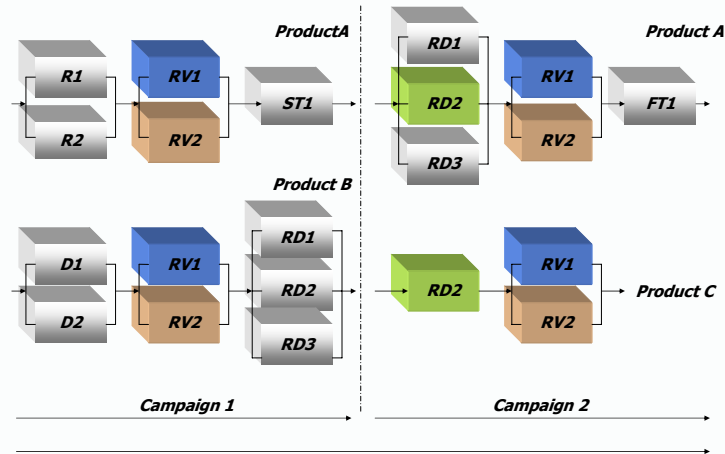
Solution of Real Problems

Flexible Process Systems

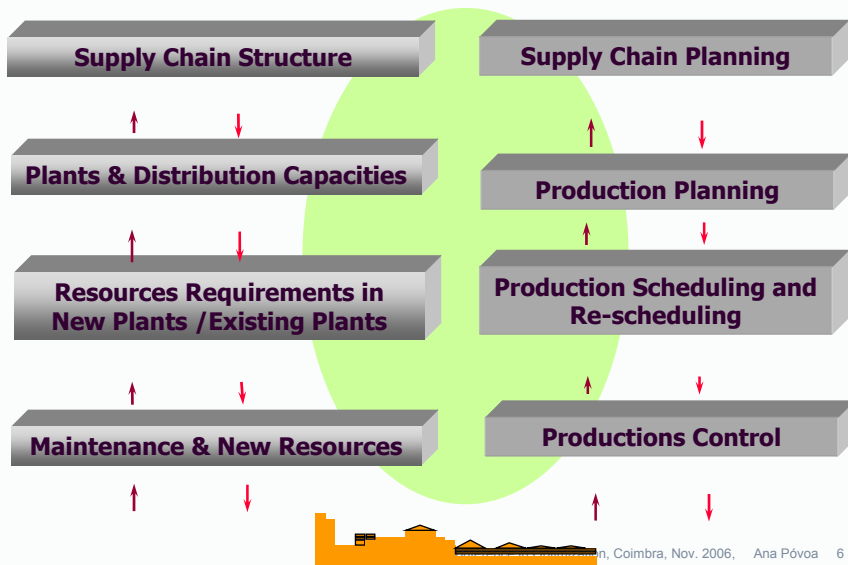
- **High variety of Products**
- **Low Volumes**
- **Batch and Semi-Continuous Operations**
- **Multipurpose Resources**



Flexible Process Systems



Flexible Process Systems : Design + Operation



Process Industries: Motivation



- Diversity of Applications
- Complex Production Processes
- Improvement of Processes Efficiency
- Client Satisfaction
- Costs Reduction



**Decision
Support
Systems**

Problems & Challenges

- How to design these plants?
- How to manage the plants resources?
- How to design and manage the associated supply chains?

SYSTEMS APPROACH → OPTIMIZATION...

The Model

- Develop the model for the problem;
 - Parameters definition
 - Sets definition
 - Variables definition
 - Binary (ex. Use or not the resource ?)
 - Continuous (ex. Batch sizes ?)
 - Constraints definitions
 - Objective definition



**Complex Optimization Problems
Mixed Integer Linear/Non-Linear
Formulations
(MILPs & MINLPs)**

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Solution Methods

- **Heuristics** – generic rules used to evaluate alternatives (FIFO, ...).
- **Meta-Heuristics** – algorithms (e.g. simulate annealing, Tabu search, Ant colony, ...).
- **Artificial Intelligence** – Ruled based methods, agent methods.
- **Constraint Programming**
- **Mathematical Programming** – MILPs and MINLPs models, use of optimization algorithms (e.g. GAMS/CPLEX, XPRESS)



Combination of Methods (Hybrid)

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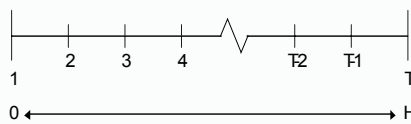
Key Components

- **Tasks** – activities that *transform* the materials:
 - Processing
 - Storage
 - Transport ...
- **Resources:**
 - Processing and storage equipments,
 - Transport
 - Man-power
 - Utilities ...
- **Time :**
 - External - Production versus external demand
 - Internal – Production Planning & Scheduling

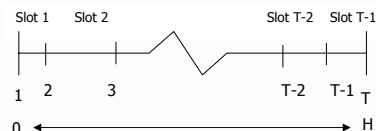
Treatment of time

- The activities (tasks) must occur such that the problem objectives are attained and no restrictions are violated
 - The use of the resources by the tasks and its availability along time must be analyzed

Discrete Time



Continuous Time



Discrete vs. Continuous Time

■ Discrete Time

- Tight mathematical formulations
- Large models – small discretisation of time
- Processing times independent of the batches.

■ Continuous Time

- Loose mathematical formulations
- Smaller models – less points within the time grid
- Time grid points determined by the model
- Processing times may be dependent of the batches

Problems Representation

(Pantelides, 2004)

Problems are very complex and very diverse ...
need a **diverse set of techniques** to match
problem characteristics

OR

Distinctions between different industrial design
& scheduling problems are not really sharp ...
uniform representations can be used

Scheduling

Given:

- ☐ Process description
- ☐ Plant flow-sheet
- ☐ Resources suitability –tasks / materials
- ☐ Operating constraints
- ☐ Production demands
- ☐ Costs/Values
- ☐ Times of operation

Determine:

- ☐ Optimal operation: scheduling

So as to:

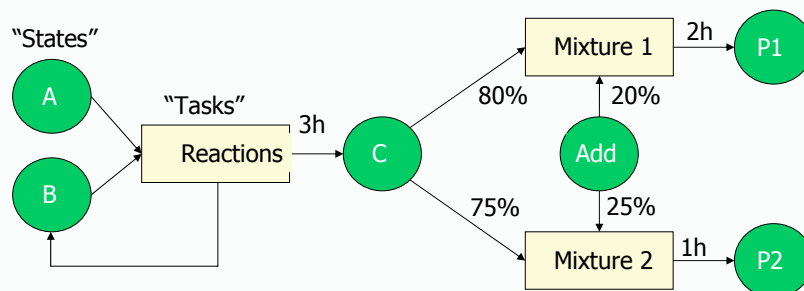
- ☐ Optimize an objective function
 Min. Delays / Max. Prod./ Min Makespan

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Process Description

State-Task Network, STN

(Kondili, Sargent & Pantelides, 1988, 1993)

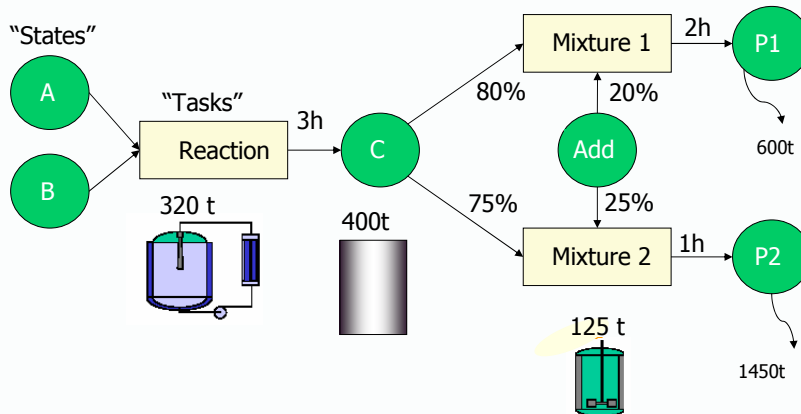


Non ambiguities in the process description:

- Sharing of intermediate products;
- Different processing alternatives;
- Recycles.

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Process + Resources + Production



How long it takes to produce ?

(adapted, Shah, 2004)

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Global Model

(Kondili et al, 1988, Shah et al 1993)

Process	→	Tasks, States, STN
Multipurpose Resources	→	Capacity & Suitability
Time representation	→	Discrete, Fixed Times
Operating Costs	→	Batch linear function
Operating modes	→	Periodic e non periodic
Operating constraints	→	Cleaning, etc. ...
Demand	→	Intervals, Fixed Values



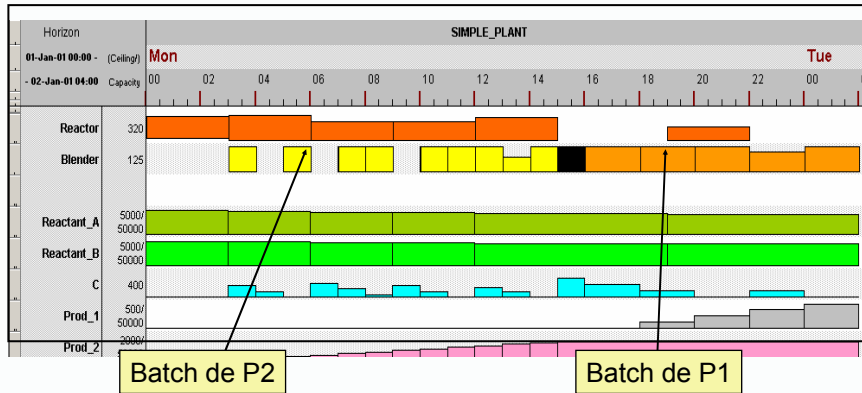
**Constraints & Objective
Function Linear**



**MILP
Problem**

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Scheduling



Answer : 26 hours

(adapted, Shah, 2003)

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STN Restrictions

- ☐ Tasks are always associated to materials that suffer transformation.
- ☐ Tasks associated to a single equipment.
- ☐ Each resource is treated independently and non uniformly
- ☐ Generalizations implies the addition of constraints



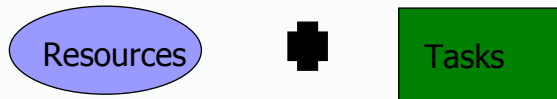
Generic Models but with some complexity

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Resource -Task Network, RTN

(Pantelides, 1994)

- Uniform treatment of all resources
 - Materials
 - Processing & Storage equipment
 - Utilities & Man-power
 - Connections
 - Transport resources ...



- Classified accordingly to its functionality
- All resources of the same class have the same functionality

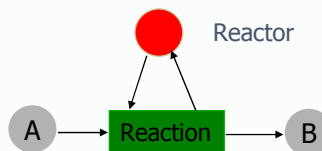
- Abstract operation that consumes & produces resources

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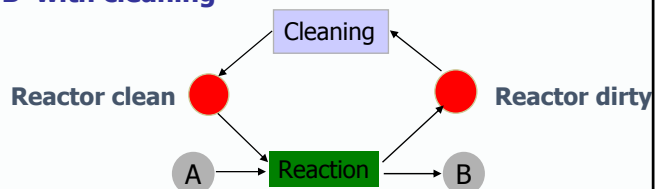
Resource-Task Network, RTN

(Pantelides, 1994)

Reaction A → B



Reaction A → B with cleaning



GENERIC & SIMPLE MODELS

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Formulations: STN versus RTN

$$MaxPR = \sum_{s \in SP} \left[(S_{s,H+1} - S_{s,0}) \cdot v_s + \sum_t D_{s,t} \cdot v_s \right]$$

s.t.

$$\sum_{i \in I_j} \sum_{t'=t-p_i+1}^t W_{i,j,t'} \leq 1 \quad \forall j, t=1, \dots, H$$

$$0 \leq S_{st} \leq C_s \quad \forall s, t=1, \dots, H$$

$$V_{ij}^{\min} W_{ij} \leq B_{ijt} \leq W_{ij} \cdot V_{ij}^{\max} \quad \forall i, j \in K_i, t=1, \dots, H$$

$$0 \leq U_{ut} \leq U_u^{\max} \quad \forall u, t=1, \dots, H$$

$$U_{ut} = \sum_i \sum_{j \in K_i} (\alpha_u W_{ij} + \beta_u B_{ijt}) \quad \forall u, t=1, \dots, H$$

$$S_{s,t} = S_{s,t-1} + \sum_{i \in I_s} \bar{\rho}_s \sum_{j \in K_i} B_{i,j,t-t_i} + \sum_{i \in I_s} \rho_u \sum_{j \in K_i} B_{i,j,t} \sum_{j \in K_i} - D_{s,t} + R_{s,t}$$

$$\forall s, t=1, \dots, H+1$$

$$S_{st}, W_{ijt}, B_{ijt}, D_{st}, R_{st}$$

$$MaxPR = \sum_{r \in RP} \left[(R_{r,H+1} - R_{r,0}) \cdot v_r + \sum_t \Pi_{r,t} \cdot v_r \right]$$

s.t.

$$0 \leq R_{rt} \leq R_{rt}^{\max} \quad \forall r, t=1, \dots, H$$

$$V_{kr}^{\min} N_{kr} \leq \xi_{kr} \leq N_{kr} \cdot V_{kr}^{\max} \quad \forall k, r \in PE_i, t=1, \dots, H$$

$$R_{r,t} = R_{r,t-1} + \sum_{k=0}^{t-1} (\mu_{kr} N_{k,t-\theta} + \nu_{kr} \xi_{k,t-\theta}) + \Pi_{rt}$$

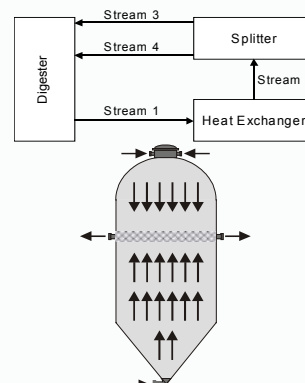
$$\forall r, t=1, \dots, H+1$$

$$R_{rt}, N_{kt}, \xi_{kt}, \Pi_{rt}$$

Scheduling: Caima Pulp Mill

(Castro, Barbosa-Póvoa e Matos, 2002)

- **Four Digesters operating in batch mode (D3, D4, D5 e D6)**
- **Vapor resource limitation**



What is the optimal digesters sequence that maximizes production while account for vapor limitations?

Scheduling: Caima Pulp Mill

(Castro, Barbosa-Póvoa e Matos, 2002)

Process:

- 1 – Chip filling;
- 2 – Acid filling
- 3 – Heating (55°C to 130°C)
- 4 – Cooking
- 5 – Degasification (high & low pressure)
- 6 - Blowing

Cyclic Operation – sequence that is repeated

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Scheduling: Caima Pulp Mill

(Castro, Barbosa-Póvoa e Matos, 2002)

**Detailed Model (gPROMS)
Cooking Operation modeling**



**RTN Model – Scheduling
Time Discretisation**

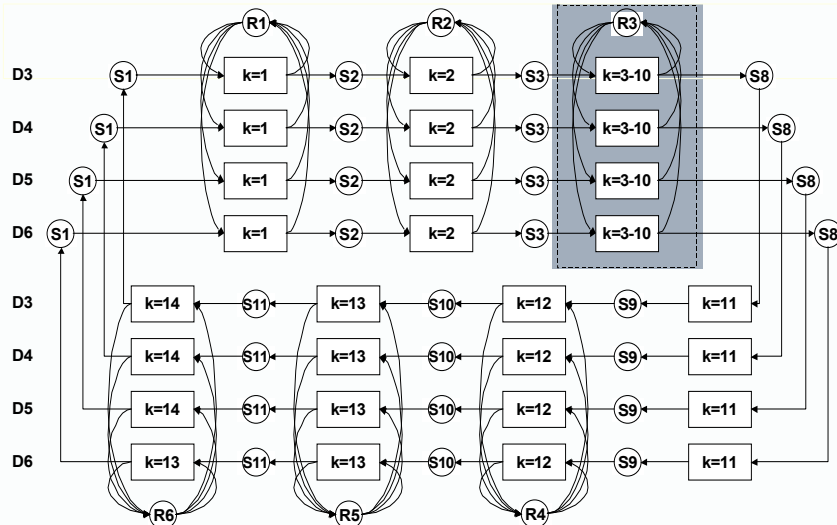


**Optimal
Sequence**

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Cooking Process, RTN

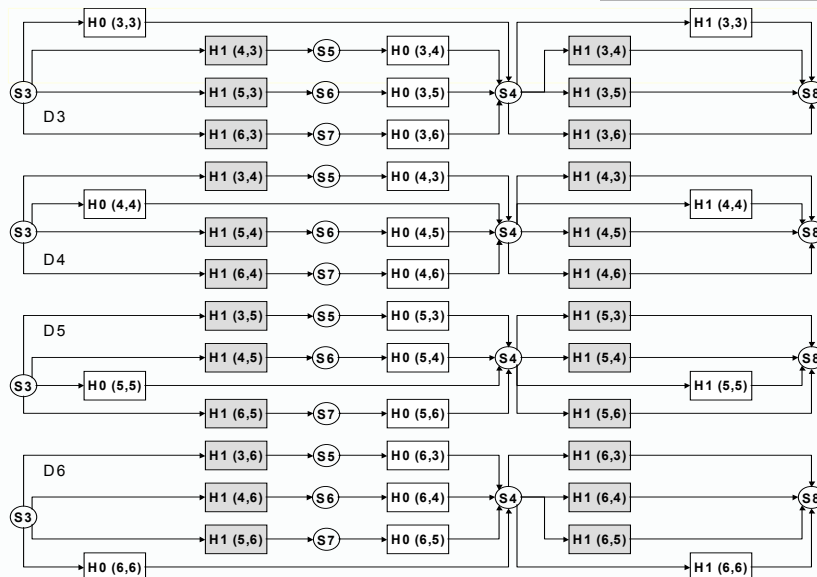
(Castro, Barbosa-Póvoa e Matos, 2002)



Heating phase simplification K=3-10

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Heating Phase, RTN (Castro, Barbosa-Póvoa e Matos, 2002)



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Scheduling: Caima Pulp Mill

(Castro, Barbosa-Póvoa e Matos, 2002)

Optimal Sequence

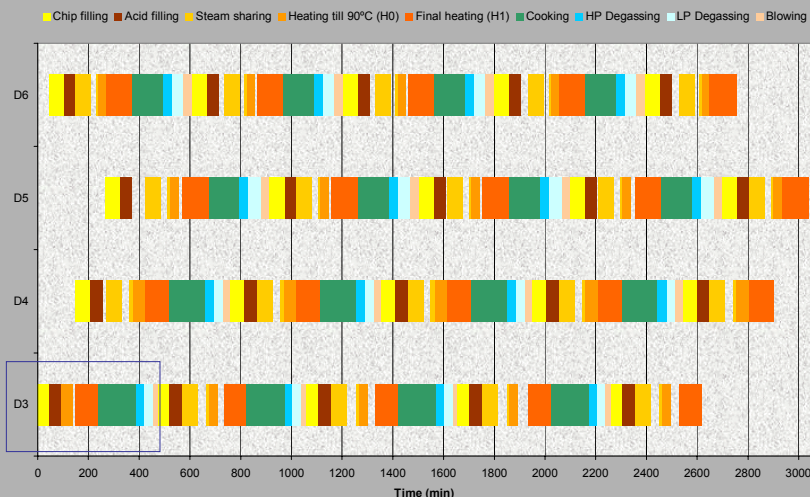
	13 t/h	14 t/h
Optimal Sequence	D3-D4-D5-D6	D3-D6-D4-D5
Cycle Time (min.)	605	595

Scenarios Study

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Optimal Scheduling for 14 ton/hr

(Castro, Barbosa-Póvoa e Matos, 2002)



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Flexible Systems Scheduling

(Shah, 1998, Floudas & Lin, 2004, Mendez et al., 2005)

- Generic & Flexible Representations
- Detailed Models

BUT IS MISSING

- Dynamic Scheduling treatment
- Uncertainty study
- Explore more efficient solution methods – complex problems
- Real cases solution

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Design / Retrofit

Given:

- ☐ Process Description
- ☐ Plant Superstructure : Equipment & Topology
- ☐ Equipment Suitability –Tasks/Materials
- ☐ Operational constraints
- ☐ Demands
- ☐ Operating & Investment Costs/Values
- ☐ Operation times

Determine:

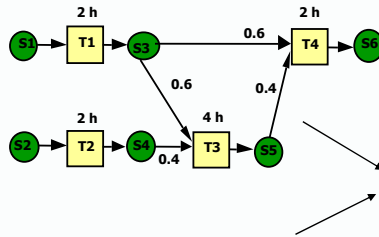
- ☐ Plant design : Equipment & Topology
- ☐ Optimal Operation : scheduling

So as to:

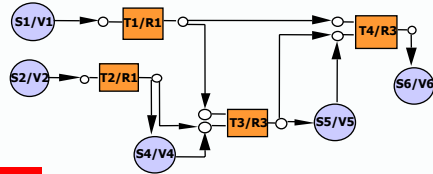
- ☐ Optimize and Objective Function
Min. Costs / Max. Profit

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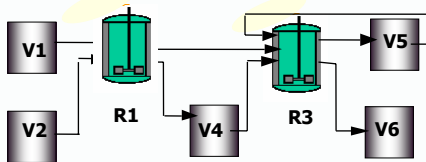
State-Task Network, STN



maximal State-Task Network, mSTN



Equipment Network, Flowsheet



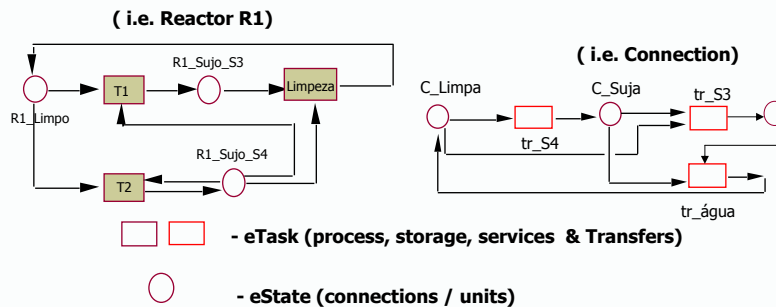
- Only feasible configurations

- Precise representation of :

- all transfers
- all material locations
- any storage policies

Equipment-Process Modeling

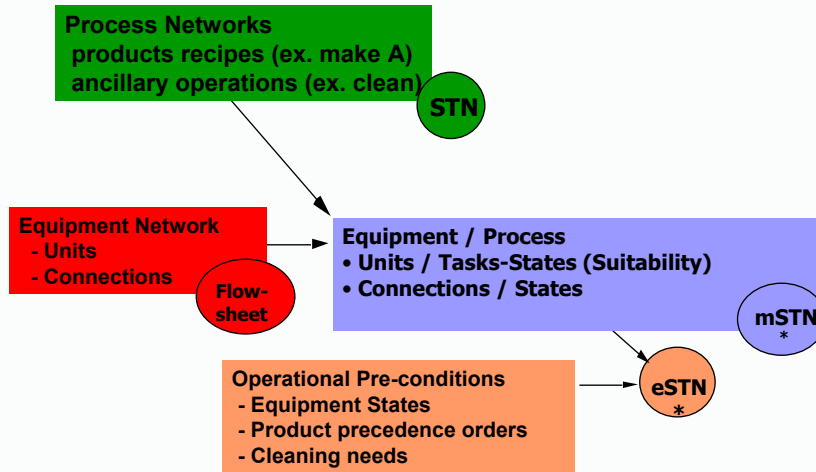
Equipment State- Task Network (eSTN)



- Define allowable states of each piece of equipment / connection (eStates)
- Define allowable transformations between equipment states caused by process, transfers, storage and cleaning tasks (eSTN Tasks)

Representing:

- precedence constraints
- sequence dependencies
- cleaning requirements



* - generated automatically

- ☐ Process Representation, STN;
- ☐ Resources with Discrete & Continuous Capacity;
- ☐ Plant Topology
- ☐ Time Discretisation;
- ☐ Short-term & Periodic Operation;
- ☐ Multipurpose Resources
- ☐ Fixed Processing Times;
- ☐ Non-preemptive Operations;
- ☐ Generic Storage Policies;
- ☐ Operating demands;
- ☐ Utility circuits;
- ☐ Multi-product operation.



**Objective
Function**



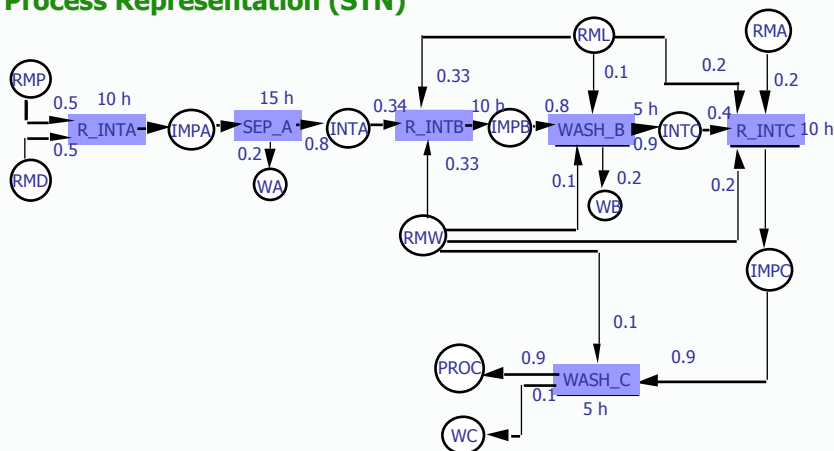
**MILP
Problem**

Expand Existence Capacity ???

If Profitable???

- How to expand ???
- How much it costs ???

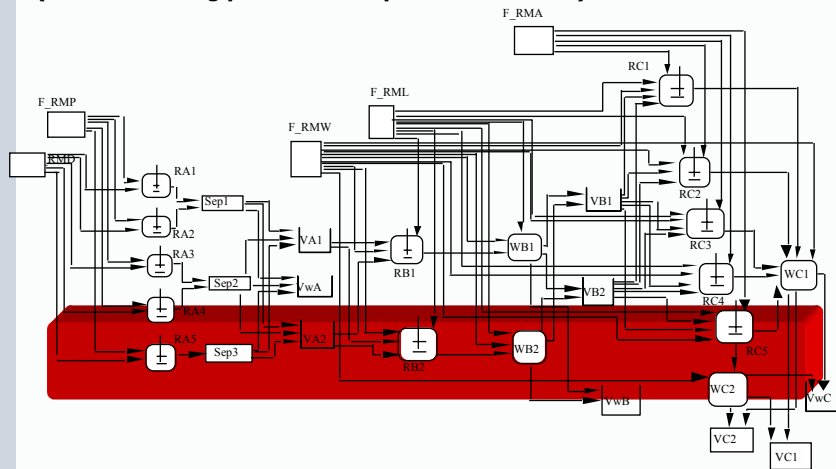
Process Representation (STN)



Retrofit: Example

(Barbosa-Póvoa, 1994)

Superstructure – Flowsheet (in black existing plant – in red possible additions)

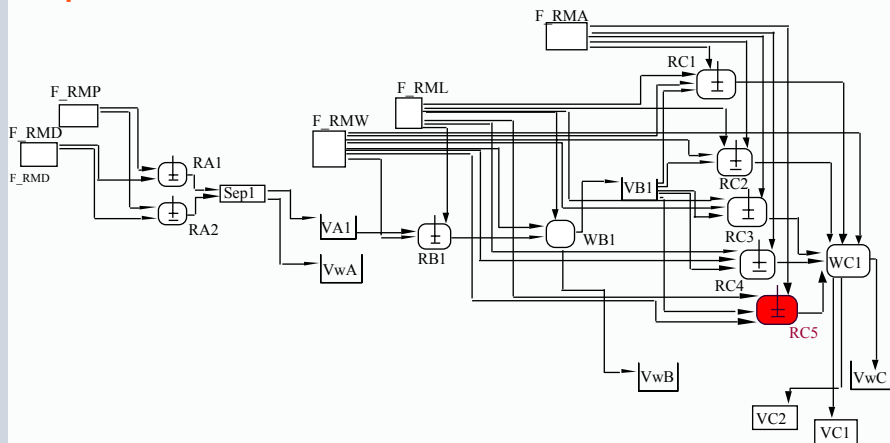


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Retrofit: Example

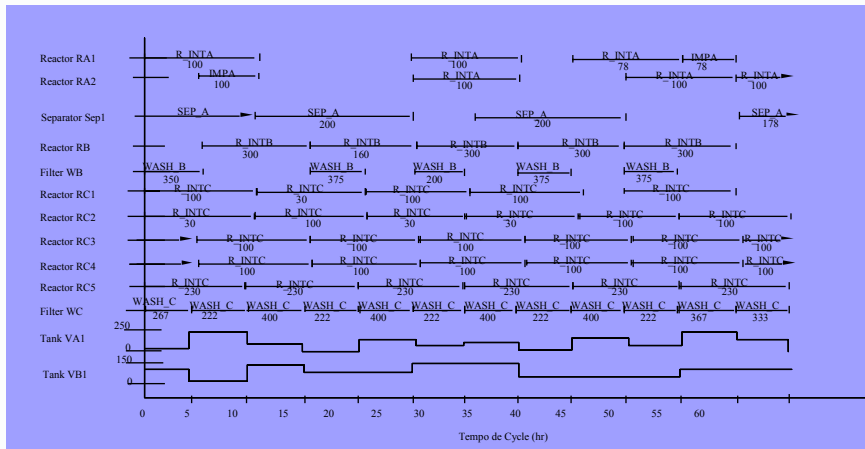
(Barbosa-Póvoa, 1994)

Optimal Structure



Profit = (> 20%)

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- Generic Models
 - Plants Topology
 - Multipurpose Resources
 - Operating Constraints
 - Discrete & Continuous Capacities
 - Cyclic & Short Term Operation
- Time
 - Discrete (Pinto, Barbosa-Póvoa e Novais, 2005)
 - Continuous (Castro, Barbosa-Póvoa e Novais, 2005)



Investment in the models applications

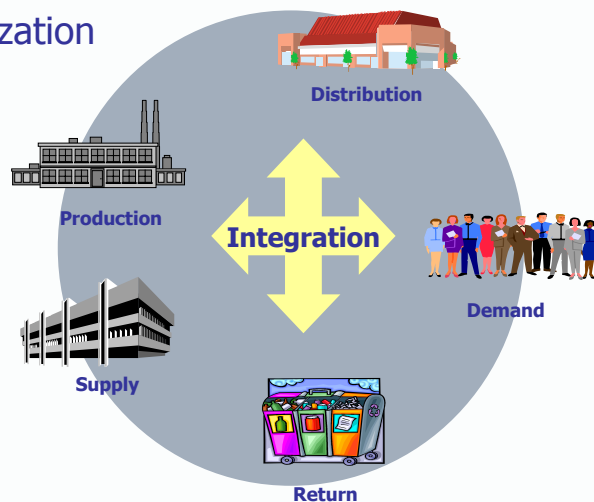
Design of Flexible Systems

(Barbosa-Póvoa, 2006)

- Details models but exists space for much more :
 - Multi-level models (design, planning & scheduling)
 - Multi-objective models
 - Uncertainty modeling
 - Explore more efficient solution methods
- Explore the solutions of real cases

Supply Chain

Optimization



Optimization Opportunities

- The supply chains are difficult to understand
- Decisions are frequently based on common sense



- Optimization tools allow the possibility of looking in an integrated form to:
 - Design & Operational decisions

Supply Chains

- Previous representations can be extended to the supply chain
- Knowledge obtained within the design and scheduling problems should be used.



- **Models**
 - Detailed and able to capture interactions
 - Deal with uncertainty
 - Dynamic & Flexible
 - Extensible

Supply Chains Operation

(Amaro e Barbosa-Póvoa, 2004, 2006)

TOPOLOGY

Chain Structure
Transportation Network



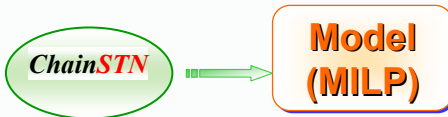
OPERATION

Tasks
Materials flows



MARKET ASPECTS

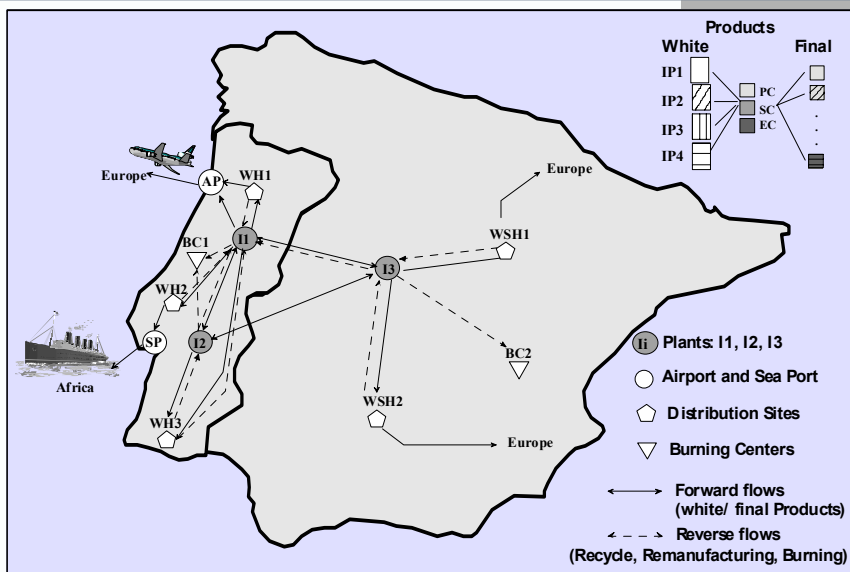
Supply/Demand
Constraints



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Closed Loop Supply Chain with return of non-conform products: Pharmaceutical Industry

(Amaro e Barbosa-Póvoa, 2006)



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Main Operations

Production – intermediate medicines production (not for sale)
involves essentially operations like:

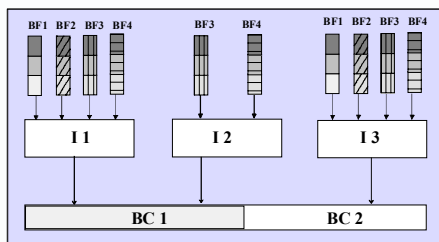
sterilization,
components calibration,
mixing, etc.

Customization – considers operations as:

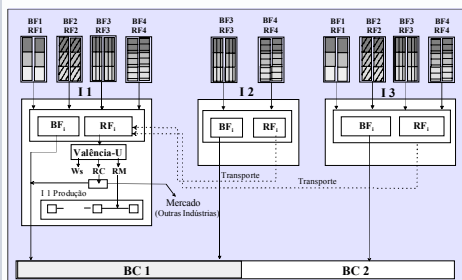
filling,
blistering,
packing, etc.

Distribution and Supply – considers operations as:

storing,
distribution.

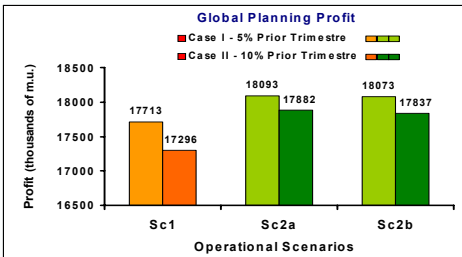


Scenario 1 – no recover,
Burning (SC1)



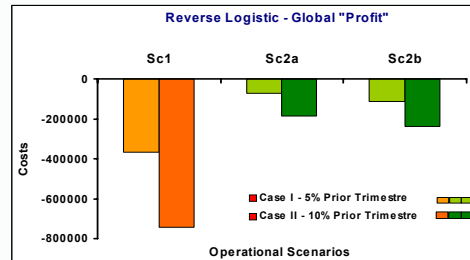
Scenario 2 – recover,
without minimums (SC2)
with minimums (SC3)

Return with and without Recover (Amaro e Barbosa-Póvoa, 2006)



Recovery of medicines is more favourable than the non-recovery situation.

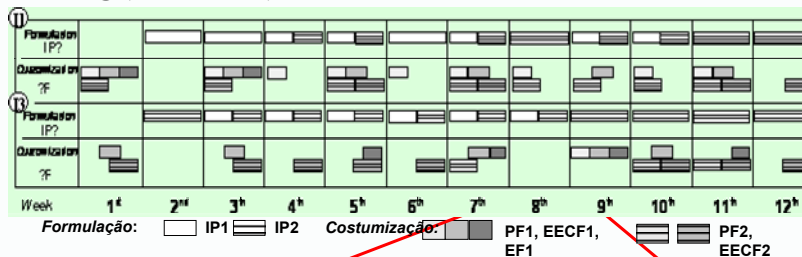
The increase of non conform products recovery reduces the chain "profit".



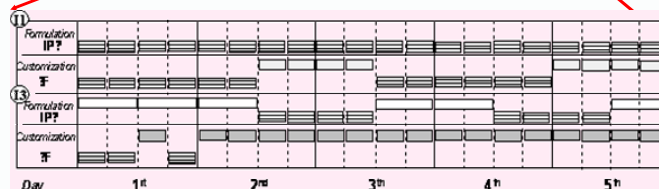
Planning & Scheduling (Amaro e Barbosa-Póvoa, 2006)

(Amaro e Barbosa-Póvoa, 2006)

Planning (Antibiotics) – 3 months



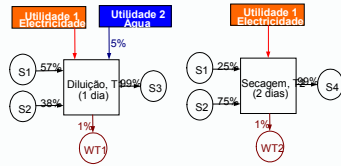
Scheduling – 5 days



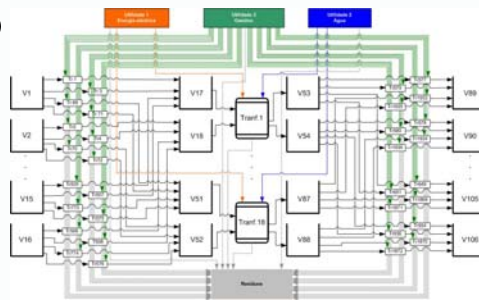
Design of a recovery network of an industrial polluted waste

(Duque, Barbosa-Póvoa e Novais, 2005, 2006)

Process



Super-estrutura



+ Environmental data

Optimize the network maximizing the profit accounting for :

- Demands within intervals
- Environmental Impacts (CTAM, CTWM, SMD...)

Design of a recovery network of an industrial polluted waste

(Duque, Barbosa-Póvoa e Novais, 2005, 2006)



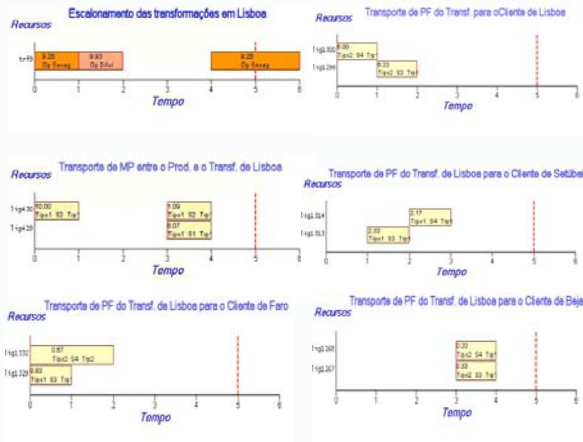
Simplified super-structure

Optimal Network

Design of a recovery network of an industrial polluted waste

(Duque, Barbosa-Póvoa e Novais, 2005, 2006)

Operation



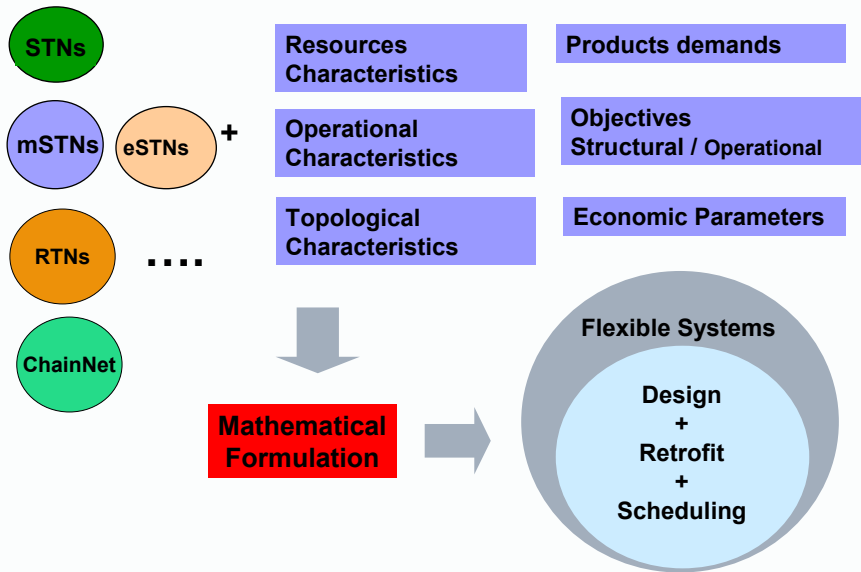
Supply Chains

(Goetschalckx et al. 2002, Shah, 2004)

Area with a great potential.
 There is some work done but there is space
 for much more:

- Improve existing structures
- Integrated different decision levels
- Explore environmental impacts
- Economic details
- Uncertainty
- Deal with complexity & different scales
-

Optimization is a possible Solution



Conclusions

- Design & Scheduling
 - Detailed models
 - Solutions of some real cases
 - There is space for more ...
- Supply Chains
 - Detail models are appearing
 - Great complexity in the modeling & solution
 - There is space for more ...

Optimization → Possible Solution

Future

- Fill the “GAP” between research & its application
- Explore solution methods more efficiently :
 - Hybrid methods
 - Heuristics + MILPs
 - Meta-Heuristics + MILPS
 - Constraint Programming + MILPs
- Integrated different decision levels
- Explore environmental impacts
- Uncertainty

Thanks

Augusto Novais, INETI
Henrique Matos, DEQB, IST

PhDs

Carlos Vieira, MSc
Cristina Amaro, MSc
Elisa Cunha, PhD
Isabel Salema, MSc
Joaquim Duque
Marta Gomes, MSc
Pedro Castro, PhD
Susana Relvas
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Ricardo Mateus, MSc
Sofia Pinheiro, MSc
Verónica Becken

Design and Scheduling of Flexible Processing Systems: An Optimization Approach

Ana Paula Barbosa Póvoa

Centro de Estudos de Gestão, CEG-IST

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References

- Amaro, C, e A.P.F.D. Barbosa-Póvoa (2006), Close Loops Supply Chains: Managing Product Recovery Portfolios, *Computer Aided Chemical Engineering*, Vol. 21B, Editores W. Marquardt e C. Pantelides, Elsevier, 1875-1880.
- Amaro, C., A.P.F.D. Barbosa-Póvoa (2004), Optimal Supply Chain Operation – A Discrete Model Formulation, *Computer Aided Chemical Engineering*, Vol. 18, Editores A. Barbosa-Póvoa e H. Matos, Elsevier, 877-883.
- Barbosa-Póvoa, A. P. F. D. (2006), A Critical Review on the Design and Retrofit of Batch Plants, em publicação, *Computers and Chemical Engineering (Comp. Chem Engng)*.
- Barbosa-Póvoa, A.P.F.D., R. Mateus e A.Q. Novais (2002), Optimal Design and Layout of Industrial Facilities: A Simultaneous Approach, *Industrial Eng. and Chem. Res.*, 41, 15, 3601-3609.
- Barbosa-Póvoa, A.P.F.D., R. Mateus e A.Q. Novais (2002), Optimal Design and Layout of Industrial Facilities: An Application to Multipurpose Batch Plants *Industrial Eng. and Chem. Res.*, 41, 15, 3610-3620.
- Barbosa-Póvoa, A.P.F.D. e S. Macchietto (1997). Design of Multipurpose Batch Plants with Operational Pre-Conditions. *Revista de Investigação Operacional*, 2,17, 113-136.
- Barbosa-Póvoa, A. P., & Macchietto, S. (1994a). Detailed Design of Multipurpose Batch Plants. *Computers & Chemical Engineering*, 18(11-12), 1013-1042.
- Barbosa-Póvoa, A. P. (1994). Detailed Design & Retrofit of Multipurpose Batch Plants. PhD, University of London.
- Chase, R. B., F. R. Jacobs e N. J. Aquilano (2005). Operations Management for Competitive Advantage with Global Cases, 11ª edição, *McGrawHill/Irwin*.
- Castro, P., A. P. F. D. Barbosa-Póvoa, e A. Q. Novais (2005), Simultaneous Synthesis, Design and Scheduling of Multipurpose Plants using RTN-based Continuous-time Formulations, *Industrial Eng. and Chem. Res.* 44, 343-357.
- Castro, P., A. P. F. D. Barbosa-Póvoa e H. Matos (2003), Optimal Periodic Scheduling of Batch Plants using RTN-based Discrete and Continuous Time: a Case Study Approach, *Industrial Eng. and Chem. Res.*, 42, 3346-3360.

Iberian Conference in Optimization, Coimbra, Nov. 2006, Ana Póvoa 62

References

- Castro, P., H. Matos e A. P. F. D. Barbosa-Póvoa (2002), Dynamic Modelling, Scheduling of an Industrial Batch System, *Comp. Chem. Eng.*, 26, 671-686
- Castro, P., A. P. F. D. Barbosa-Póvoa e H. Matos (2001), An improved RTN continuous-time formulation for the short-term scheduling of multipurpose batch plants, *Industrial Eng. and Chem. Res.*, 40, 2059-2068.
- Crooks, C., (1992) Synthesis of Operating Procedures for Chemical Plants. PhD Thesis, Imperial College of Science Technology and Medicine, University of London.
- Duque, J, A.P.F.D. Barbosa-Póvoa e A.Q. Novais (2006), Case-Study of a Regional Network for the Recovery of Hazardous Materials, *Computer Aided Chemical Engineering*, Vol. 21B, Editores W. Marquardt e C. Pantelides, Elsevier, 1797-1792.
- Duque, J., A.P.F.D. Barbosa-Póvoa e A.Q. Novais (2005), Synthesis and Optimisation of the Recovery Route for Residual Products with Uncertain Product Demands, em publicação no *Computers and Operational Research*, disponível na web desde Julho 2005.
- Dedopoulos, I.T. and N. Shah (1995), Preventive Maintenance Policy Optimisation for Multipurpose Plant Equipment, *Comput. chem. Engng*, **S19**, S693-S698.
- Floudas, C. A., e Lin, X. (2004), Continuous versus Discrete time formulations approaches for scheduling of chemical processes, *Comp. Chem. Engng.*, 28, 2109-2129.
- Giannellos, M.F., e Georgiadis, M.C. (2002). A simples continuous time formulation for short term scheduling of multipurpose batch plants, *Ind. Engn. Chem. Res.*, 41, 2178-2184.
- Goetschalckx, M., C.J. Vidal and K. Dogan, 2002, Modelling and design of global logistics systems: A review of integrated strategic and tactical models and design algorithms, *European Journal of Operational Research (EJOR)*, 143, 1-18.
- Grossmann, I.E. (2005), Enterprise-Wide Optimization: A new frontier in Process Systems Engineering, *AIChE Journal*, 1846-1857.

Iberian Conference in Optimization, Coimbra, Nov. 2006, Ana Póvoa 63

References

- Ierapetritou, M. G.; Floudas, C. A. (1998) Effective Continuous-Time Formulation for Short-Term Multipurpose Batch Processes, *Ind. Engng. Chem. Res.*, 37, 4341.
- Janak, S.L, Lin, X., e Floudas, C.A. (2004) Enhanced Continuous time unit specific event based formulation for short term scheduling of multipurpose batch processes: resource constraints and mixed storage policies. *Ind. Eng. Chem Res.*, 44, 426.
- Kondili, E., Pantelides, C.C., Sargent, R. W. (1993), A General Algorithm for short-term scheduling of batch operations, *Comp. Chem. Engn.*, 2, 211-227.
- Lin & Floudas, C. A. (2001), Design and Scheduling of multipurpose batch plants via an effective continuous time formulation, *Comp. Chem. Engn.* 25, 665-674.
- Maravelias, C. T., e Grossmann, I.E. (2003) New general continuous time state-task network formulation for short term scheduling of multipurpose batch plants, *Ind. Engn. Chem Res*, 42, 3056-3074.
- Mendez, C., Cerda, J., Grossmann, I., Harjunksoski, I., Fahl, M. (2006), State of the Review of Optimisation Methods for Short-Term Scheduling of Batch Processes, *Computers & Chem. Engn.*, 30, 6/7, 913-946.
- Pantelides, C.C. (2004), Unified Frameworks for Optimal Process Planning and Scheduling, FOCP0, USA.
- Papageorgaki, S. and Reklaitis, G. V. (1990). "Optimal Design of Multipurpose Batch Plants 1. Problem Formulation", *Ind. Eng. Chem. Res.*, 29, 10, 2054-2062.
- Papageorgiou, L.G. and C.C. Pantelides, (1996) "Optimal Campaign Planning/Scheduling of Multipurpose Batch/Semicontinuous Plants. 1. Mathematical Formulation", *Ind. Eng. Chem. Res.*, **35**, 488-509.
- Papageorgiou, L. and Pantelides, C. C. (1994). "Optimal Scheduling of Heat-Integration Multipurpose Batch Plants", *Ind. Eng. Chem. Res.*, 33, 12, 3168-3186.
- Pinto, T., A.P.F.D. Barbosa-Póvoa e A.Q. Novais (2005), Optimal Design and Retrofit of Batch Plant with a Periodic Mode of Operation, *Comp. Chem. Engng*, 29, 1293-1304.

Iberian Conference in Optimization, Coimbra, Nov. 2006, Ana Póvoa 64

References

- Pinto, T., A.P.F.D. Barbosa-Póvoa e A.Q. Novais (2003), Optimal Design of Heat-Integrated Multipurpose Batch Facilities with Economic savings in Utilities: A Mixed Integer Mathematical Formulation, *Annals of Operations Research*, 120,201-230.
- Reklaitis, G. V. (1989). Progress and Issues in Computer Aided Batch Process Design., *Third International Conference on Foundations of Computer- Aided Proc. Des. (FOCAPD)*, pp. 241-276.
- Schilling, G. and Pantelides, C. (1996). A Simple Continuous-Time Process Scheduling Formulation and a Novel Solution Algorithm. *Comp. Chem. Eng.*, 20, S1221-S1226.
- Shah, N (2004), *Process Industries Supply Chains: Advances and Challenges*, *Computer-Aided Chemical Engineering*, 18, Edts. A. Barbosa-Póvoa and H. Matos, Elsevier, 123- 138.
- Shah, N. (2003), Making things better: systems approaches for improved processes and supply chains Inaugural Lecture, Imperial College, London
- Shah, N., (1998), Single and Multisite Planning and Scheduling: Current Sytatus and Future Challenges. In *Third International Conference on Foundations of Computer- Aided Proc. Operations. (FOCAPo)*, 75-90.
- Shah, N., C.C. Pantelides and R.W.H. Sargent (1993) Optimal Periodic Scheduling of Multipurpose Batch Plants. *Annals of Operations Research*, 42, 193-228.
- Slack, N, Chambers, S., Harrison, A., Johnston, R. (1995), *Operations Management*, Pitman Publishing, London, U.K.
- Sundaramoorthy, A.; Karimi,(2005) I.A. A simpler better slot-based continuous-time formulation for short-term scheduling in multipurpose batch plants. *Chem. Eng. Sci.* 60, 2679.
- Zhang, X., e Sargent, R.W. (1996) The Optimal Operation of Mixed Production Facilities – a general formulations and some approaches for the solution, *Computers & Chem Engn.*, 20. 897-904.